

## LIFT STATION CALCULATIONS

for

## **FIRE STATION #7**

City of Fellsmere, Florida

September 2022 Revised May 2023

> Prepared by: MBV Engineering, Inc. 1835 20th Street Vero Beach, Florida 32960 Phone: 772-569-0035

> > Certificate of Authorization #: 3728

Engineer's Project Number: 22-0492 Designed by: TJH

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## Lift Station Design Summary Sheet

#### - Fiberglass Wet Well

Diameter =	6.0 ft
Depth =	7.7 ft

- Concrete Anti-flotation Ballast: Volume = 0.0 Cu.Yd.
- Discharge Line 4.00 in DIA PVC Force Main
- Design Operating Points:

Flow =	78.3 gpm
TDH =	82.8 ft

 Operating Points:

 Flow =
 92.0 gpm

 TDH =
 89.8 ft

- Pump Selection:

Two - Sulzer PIR - PE45/2C 6.7 hp 230V 3P 60Hz 3525 RPM 6.3 inch Impeller

- For Details of System Head curve generation, buoyancy calculation and pump selection, please reference the attached calculations, head curves, and pump data sheet.

#### 1. PURPOSE

The purpose of this report is to provide the local Utility Department and the Florida Department of Environmental Protection (FDEP) with documentation and calculations in order to construct a proposed lift station and force main to the existing system. The calculations contained in this report demonstrate the system is designed to meet the requirements of FDEP and the local Utility Department.

#### 2. DESIGN FLOW DETERMINATION

FLOW SOURCE	TYPE	NUMBER	UNIT FLOW (gpd)	UNITS	TOTAL FLOW (qpd)
Fire Station	Institutional	3	250	per ERU	750
					0
					0
					0
					0
TOTAL					0
TOTAL					750
HOURS OF OPERATION: TOTAL (gpd/gpm): POPULATION EQUIVALENT (000'S): PEAKING FACTOR: PEAK FLOW (gpm):	24.0 HRS (Average	)	750	/	0.5 0.0 4.00 2.1
3. TRIBUTARY FLOW FROM OTHER	LIFT STATIONS				
Station Number 1 2 3	D	esign Flow (gpn 0 0 0	n)		

TOTAL DESIGN FLOW THIS STATION (GPM):

6.00 (6 gpm minimum)

#### 4. WET WELL SIZING CALCULATIONS

ENTER MINIMUM CYCLE TIME (min):	15.00
DESIGN OUT FLOW (gpm):	6.00
MINIMUM WET WELL STORAGE (gal) = Cylcle Time * Design Out Flow / Peak Factor	22.50
MINIMUM PUMPING TIME AT 0 INFLOW (min):	5.00
WET WELL DIAMETER (ft):	6.00
REQUIRED OPERATING RANGE (ft):	0.11

#### 5. DETERMINE CONTROL ELEVATIONS

TOP OF LIFT STATION ELEVATION: LOWEST GRAVITY INLET INVERT ELEVATION: ALARM INTERVAL / ELEVATION: LAG PUMP INTERVAL / ELEVATION: LEAD PUMP INTERVAL / ELEVATION: SHUTOFF INTERVAL / ELEVATION: BOTTOM OF LIFT STATION ELEVATION:

			25.50
			20.99
	0.50	/	20.49
	0.50	/	19.99
	0.50	/	19.49
= 0.11, Use:	0.14	/	19.35
			17.85

#### 6. TOTAL DESIGN HEAD CALCULATION

#### MINOR LOSSES COEFFICIENT DETERMINATION

T					
_	DISC	HARGE	COMN	/ION #1	
Eq. Length	Number	Eq. Length	Number	Eq. Length	
Based on pipe siz	ze)	Total		Total	
10.0	8	80	0	0	
5.0	8	40	0	0	
7.0	2	14	0	0	
24.0	0	0	0	0	
0.0	0	0	0	0	
22.0	3	66	0	0	
110.0	0	0	0	0	
58.0	0	0	0	0	
2.3	3	6.9	0	0	
26.0	2	52	0	0	
43.0	0	0	0	0	
Total Equivaler	nt Length (ft) =	258.9		0	
25 SIZES 2"	2_1/2"	2"	۸"	6"	8"
2	2-1/2	80	4	15.0	20.0
2.5	0.5	2.0	10.0 5.0	7.1	20.0
2.5	3.0	5.0	7.0	11.0	9.4 14.0
13.0	4.2	18.0	24.0	37.0	30.0
10.0	5.0	10.0	24.0	57.0	53.0
12.0	14.0	17.0	22.0	31.0	40.0
55.0	67.0	82.0	110.0	160.0	220.0
28.0	33.0	42.0	58.0	83.0	110.0
12	14	17	23	3.5	4.5
13.0	16.0	20.0	26.0	39.0	52.0
		-0.0		00.0	02.0
	Eq. Length Based on pipe sit 10.0 5.0 7.0 24.0 0.0 22.0 110.0 58.0 2.3 26.0 43.0 Total Equivaler be sizes 2" 5.5 2.5 3.5 13.0 4.0 12.0 55.0 28.0 1.2 13.0	$\begin{array}{c c c c c c c c c c c c c c c c c c c $	$\begin{array}{ c c c c c c } \hline & DISCHARGE \\ \hline Eq. Length & Number & Eq. Length \\ \hline Based on pipe size) & Total \\ \hline 10.0 & 8 & 80 \\ \hline 5.0 & 8 & 40 \\ \hline 7.0 & 2 & 14 \\ 24.0 & 0 & 0 \\ 0.0 & 0 & 0 \\ 22.0 & 3 & 66 \\ 110.0 & 0 & 0 \\ 22.0 & 3 & 66 \\ 110.0 & 0 & 0 \\ 23.3 & 6.9 \\ 26.0 & 2 & 52 \\ 43.0 & 0 & 0 \\ \hline 7otal Equivalent Length (ft) = 258.9 \\ \hline De sizes & 2" & 2-1/2" & 3" \\ \hline 5.5 & 6.5 & 8.0 \\ 2.5 & 3.0 & 3.8 \\ \hline 3.5 & 4.2 & 5.2 \\ 13.0 & 15.0 & 18.0 \\ \hline 4.0 & 5.0 & \\ \hline 12.0 & 14.0 & 17.0 \\ \hline 55.0 & 67.0 & 82.0 \\ 28.0 & 33.0 & 42.0 \\ \hline 1.2 & 1.4 & 1.7 \\ \hline 13.0 & 16.0 & 20.0 \\ \hline \end{array}$	$\begin{array}{ c c c c c } \hline & DISCHARGE & COMN \\ \hline Eq. Length & Number & Eq. Length & Number \\ \hline Based on pipe size) & Total \\ \hline 10.0 & 8 & 80 & 0 \\ \hline 5.0 & 8 & 40 & 0 \\ \hline 5.0 & 8 & 40 & 0 \\ \hline 7.0 & 2 & 14 & 0 \\ 24.0 & 0 & 0 & 0 \\ 0.0 & 0 & 0 & 0 \\ 22.0 & 3 & 66 & 0 \\ 110.0 & 0 & 0 & 0 \\ 22.0 & 3 & 66 & 0 \\ 110.0 & 0 & 0 & 0 \\ 23.3 & 3 & 6.9 & 0 \\ 26.0 & 2 & 52 & 0 \\ 43.0 & 0 & 0 & 0 \\ \hline 7.0 & 2 & 52 & 0 \\ 43.0 & 0 & 0 & 0 \\ \hline Total Equivalent Length (ft) = 258.9 \\ \hline be sizes & & & & \\ \hline 2'' & 2-1/2'' & 3'' & 4'' \\ \hline 5.5 & 6.5 & 8.0 & 10.0 \\ 2.5 & 3.0 & 3.8 & 5.0 \\ 3.5 & 4.2 & 5.2 & 7.0 \\ 13.0 & 15.0 & 18.0 & 24.0 \\ \hline 4.0 & 5.0 & & & \\ \hline 12.0 & 14.0 & 17.0 & 22.0 \\ \hline 55.0 & 67.0 & 82.0 & 110.0 \\ \hline 28.0 & 33.0 & 42.0 & 58.0 \\ \hline 1.2 & 1.4 & 1.7 & 2.3 \\ \hline 13.0 & 16.0 & 20.0 & 26.0 \\ \hline \end{array}$	$\begin{bmatrix} \\ \hline \\ Eq. Length & Number & Eq. Length & Total &$

### 7. HEAD LOSS DETERMINATION

PIPE: Design Flow (gpm) : Pipe Diameter (inches): Minimum Velocity (fps): Minimum Required Flow at Min. Velocity (gpm):	DISCHARGE 2.1 4.00 2.00 78.3	COMMON #1 0 8 0
Minimum Flow required for this project (gpm): Resulting Head from Minimum Flow (ft):	<b>78.3</b> 82.8	
Actual Pipe Length (ft): Equivalent Pipe Length from above (ft): TOTAL PIPE LENGTH (ft): Hazen-Williams Coefficient (Chw): Maximum Field Pressure (PSI): HEAD @ POINT OF CONNECTION	3409 258.9 3668 120 25.0 *PSI PRO 57.75	0 120 VIDED BY Jesse Roland - 5/13/2022
HIGH POINT ELEVATION: LOW WET WELL ELEVATION: AVE. STATIC HEAD:	24.00 19.35 62.40	

#### **8. SYSTEM HEAD CURVE GENERATION**

SET INITIAL FLOW (gpm): SET INCREMENTAL FLOW (gpm):		0 10	
PUMP SELECTION:	Two - Sulzer PIR - PE45/2C 6.7 hp 230V 3P 60Hz 3525 RPM 6.3 inch Impeller		
		Т	0

		•			Total Design	
	Flow (gpm)	Velocity (fps)	Friction	Static	Head	
-	0	0.0	0.000	62.400	62.4	
	10	0.3	0.452	62.400	62.9	
	20	0.5	1.629	62.400	64.0	
	30	0.8	3.449	62.400	65.8	
	40	1.0	5.872	62.400	68.3	
	50	1.3	8.873	62.400	71.3	
	60	1.5	12.432	62.400	74.8	
	70	1.8	16.535	62.400	78.9	
	80	2.0	21.168	62.400	83.6	
	90	2.3	26.321	62.400	88.7	
	100	2.6	31.986	62.400	94.4	
	110	2.8	38.154	62.400	100.6	
	120	3.1	44.817	62.400	107.2	
	130	3.3	51.971	62.400	114.4	
_	140	3.6	59.607	62.400	122.0	
Operating Point =	92	2.3	27.414	62.400	89.8	
<u>9. ACTUAL CYCLE TI</u> T= VOL [ 1/Qin + (1/ (	<u>ME:</u> Qout - Qin)]:	Average, T= Peak, T=	20.06 5.28	min min	lume (on to off)= Q average = Q peak =	29.59 1.50 6.00

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gal gpm gpm

#### **10. FDEP PUMP STATION DATA**

TYPE OF UNIT	# of UNITS	POPULATIO N PER UNIT	TOTAL POPULATION	PER CAPITAL FLOW	TOTAL AVERAGE DAILY FLOW	PEAK HR FLOW
Single-Family Home			0		0.0 GPD	
Mobile Home			0		0.0 GPD	
Apartment			0		0.0 GPD	
Commercial, Institutional or Industrial			0		0.0 GPD	
TOTAL	l				0.0 GPD	
LOCATION	TYPE		MAXIMUM	AVERAGE	MINIMUM	OPERATING CONDITIONS
TOTAL						

#### **11. BOUYANCY CALCULATIONS**

ENTER TYPE OF WELL:	С	(F=FIBERGLASS, C=CONCRETE)
VOLUME:		
WELL DEPTH: WELL DIAMETER: WELL VOLUME: WALL THICKNESS: BASE THICKNESS: BASE WIDTH:	7.7 6.0 216 8 18 10	ft (Depth) ft (D) ft <sup>3</sup> inches inches ft
FORCE OF BOUYANCY (F <sub>b</sub> ): DENSITY: F <sub>b</sub> :	62.4 13,490	lbs/ft <sup>3</sup> (WATER) lbs = volume of wet well x density of water = (3.14xD^2 /4) x Depth x 62.4
WET WELL WEIGHT (See Sketch nex DENSITY:	t page) 150	lbs/ft <sup>3</sup> (CONCRETE)
WALLS: <u>BASE:</u> TOTAL: BALLAST: TOTAL WEIGHT:	16,014 17,663 33,677 - 33,677	lbs = volume of walls x density of walls (based on conc. or fiberglass) * lbs = volume of base x density of base (based on conc. or fiberglass) ** lbs = weight of walls plus weight of base lbs 0.00 cy conc lbs
Wet Well Weight - Bouyancy Force =	20,186	lbs = 2.5 factor of safety

\* = [ (3.14 x (D+2W)^2)/4 - (3.14 x (D^2)/4) ] x Well Depth x Density \*\* = [ (3.14 x Base Width^2)/4 ] x Base Thickness x Density

#### **CONCRETE WET WELL**



# Product description



Pos.no	Description	Item no.	Quant.
	PIR PE1 60 HZ		
	Centrifugal pump: PIR PE45/2-C-60HZ PIR PE1 Submersible grinder pump type ABS Piranha with shredd reliable and economical discharge of effluent under press diameter discharge lines in communal schemes. For effluent removal from houses in rural areas where high ground must be overcome, or where only sma can be laid, and for example removal from motorway serv camp sites, large construction sites, urban renewal and re Pumped medium: sewage and other heavily polluted was Pumps of the Piranha-PE series have been designed for	ing action used for ure, using small all diameter pipework vice stations and enovation of buildings. te water. continuous operation S1 when either subme	1 erged or dry-
	installed. Piranha-S has been designed for intermittent use only (S	3, 25%) when dry installed	
	Capacity up to Head, max.	30 m3/h 75 m	
	Type: PIR PE45/2-C-60HZ PIR PE1 Technical data Delivery rate Delivery head Hydr. efficiency Shaft power Speed Impeller type Motor output Voltage Frequency Discharge outlet	: 3525 rpm : 3525 rpm : Macerator : 6.705 hp : 230 V : 60 Hz : DN32	



# PIR PE1 60 HZ



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